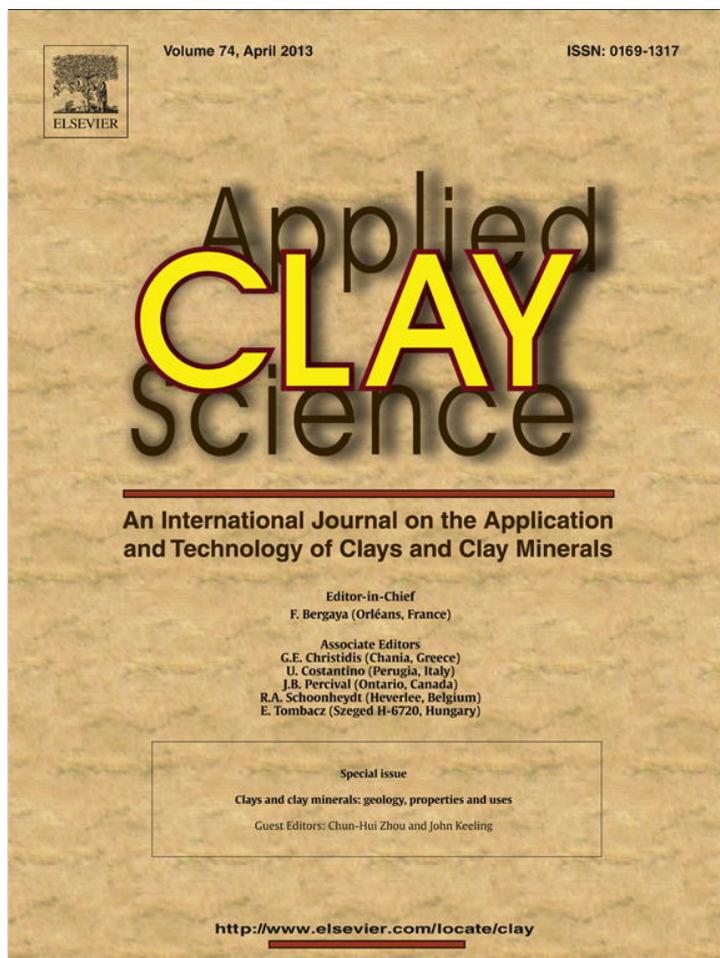


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Research paper

Natural zeolite from Pacitan Indonesia, as catalyst support for transesterification of palm oil

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ABSTRACT

The transesterification of palm oil to methyl esters (biodiesel) was studied using KOH/zeolite as solid heterogeneous catalysts. Various process variables such as KOH concentration and reaction time were studied in order to obtain maximum yield of biodiesel. A series of KOH/zeolite catalyst was prepared by impregnation of zeolite from Pacitan with potassium hydroxide in a various concentration (25 g KOH in 100 mL of distilled water; 50 g KOH in 100 mL of distilled water; 75 g in 100 mL of distilled water; and 100 g in 100 mL of distilled water). The weight ratios between zeolite and KOH solution were 1:4. Transesterification was carried out at various reaction times (1 to 4 h). The impregnation of zeolite with KOH concentration of 100 g/100 mL gave maximum yield of biodiesel. The natural zeolite, catalyst, and spent catalysts were characterised by using several techniques such as XRD, EDX, and SEM.

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1. Introduction

Petroleum-based fuel is still the main source of energy used by all countries in the world. Extensive uses of this un-renewable fuel cause the depletion of petroleum-based fuel sources. Various kinds of alternative energy sources have been explored (Zhou et al., 2011), and one of them is biodiesel. Biodiesel has been considered as an alternative source of petroleum-based fuel due to its similarity to petroleum-based diesel (Noiroj et al., 2009). Chemically, biodiesel is a mixture of methyl esters with long-chain fatty acids that can be produced through transesterification process of vegetable oils and animal fats (Leung et al., 2010). This process is usually carried out in the presence of a homogeneous base or acid catalysts in order to reduce the reaction temperature and to control the product selectivity (Benjapornkulaphong et al., 2009). In the homogeneous method, the reactants, catalyst, and FAME are all in the liquid phase, which is difficult to separate the catalyst from the after-reaction product (Kansedo et al., 2009). On the other hand, homogeneous base catalysts such as sodium hydroxide cannot be recovered or regenerated after the reaction and also produce toxic wastewater (Soetaredjo et al., 2011). Solid catalysts are a new choice to replace the liquid homogeneous catalyst due to its advantages such as less corrosive, easier to handle and separate, reusable and generating less amount of toxic wastes (Helwani et al., 2009).

Recently, there has been increasing development of heterogeneous catalyst. Solid catalysts that have been studied and used for transesterification of vegetable oils including alkali and alkali earth metal supported on Al_2O_3 (Benjapornkulaphong et al., 2009; Noiroj et al., 2009), alum (Aderemi and Hameed, 2009), K_2CO_3 supported on alumina/silica (Lukic et al., 2009), calcium oxide (Boey et al., 2009), calcium-zinc mixed oxide (Ngamcharussrivichai et al., 2008), quick lime bit (Kouzu et al., 2009), mesoporous molecular sieves MCM-41 (Carmo et al., 2009), and KOH supported on bentonite (Soetaredjo et al., 2011), etc. However, the drawback of using solid materials as catalyst for biodiesel production, especially the synthesized ones, is on its price. To reduce the cost of production, the solid catalyst should be low in price, and available in large quantity.

Zeolite is a crystalline aluminosilicate with a three-dimensional framework structure that forms uniform pore size (Cejka et al., 2007). Because of its important chemical properties, this material has been applied in many industrial application such as selective absorbent, ion-exchange resin, and high activity catalyst (Xia et al., 2011; Zhang et al., 2010; Zhou, 2010, 2011). Various kinds of solid materials as mentioned in previous paragraph have been used as heterogeneous catalyst or catalyst supports in biodiesel production, but study about the utilization of natural clay materials such as zeolite as catalyst or catalyst support for biodiesel is still scarce.

The present work was focused in modification of natural zeolite-supported KOH prepared through impregnation method as catalyst for transesterification of palm oil. In this study, we used natural zeolite from Pacitan (East Java, Indonesia). To the best of our knowledge, there is no information available about the utilization of natural zeolite as catalyst or catalyst support for biodiesel production. In the present

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study, the zeolite was used as catalyst support; the effects of KOH loading and transesterification conditions on the yield of biodiesel were also studied.

2. Materials and methods

2.1. Materials

Natural zeolite used in this study was obtained from Pacitan, East Java, Indonesia. Prior to use, natural zeolite was crushed using a JANKE & KUNKEL micro hammer mill to obtain zeolite with particle size of 170/240 mesh. Subsequently, the zeolite was treated with 30% of hydrogen peroxide solution to remove the organic impurities. Excess hydrogen peroxide solution was removed by gently heating in a water bath, and the solution was separated from the zeolite. Subsequently, the purified zeolite was repeatedly washed and dispersed in distilled water. After the water have been separated from zeolite, the purified zeolite was then dried in an oven at 110 °C for 24 h to remove moisture content from its structure. The dried zeolite was finally crushed in a micro hammer mill to obtain powder zeolite with particle size of 170/240 mesh.

For transesterification study, the refined palm oil (Bimoli) was purchased from local market, while analytical grade methanol, potassium hydroxide, and n-hexane were obtained from Merck, Darmstadt, Germany. The standard fatty acid methyl ester for FAME analysis was purchased from Sigma Aldrich (Singapore).

2.2. Catalyst preparation

A series of zeolite catalysts was prepared by impregnation with KOH at different KOH concentrations. A brief procedure of catalyst preparation is as follows: a known amount of KOH (25, 50, 75, and 100 g) was added into 100 mL distilled water, followed by the addition of zeolite powder into the solution. The weight ratio between zeolite and KOH solution was 1:4. Afterwards, the mixture was removed to three-neck flask equipped with reflux condenser. The mixture of zeolite and KOH solution was stirred at 60 °C for 24 h. Subsequently, zeolite and KOH solution was separated by filtration using a vacuum filter system. The zeolite catalyst was then oven-dried at 110 °C for 24 h, and calcined in a furnace at 450 °C for 4 h.

2.3. Material and catalyst characterization

Natural zeolite and catalysts were characterized using several methods such as X-ray Diffraction analysis, Energy-Dispersive X-ray (EDX) spectrometry, and scanning electron microscopy (SEM). The X-ray Diffraction analysis was conducted using a Philips X-pert Powder Analytical diffractometer, and as a source for $\text{CuK}\alpha$ radiation (1.54056 Å) a 2.2 kW Cu anode was used. The XRD pattern was obtained at operating condition 40 kV and 40 mA with 2θ measurements between the ranges of 5° to 90°.

Since potassium plays an important role in transesterification of palm oil into biodiesel, the potassium content both in raw zeolite and catalyst was determined by an Energy-dispersive X-ray (EDX) spectrometry (Shimadzu EDX-720/800HS). EDX was used in conjunction with scanning electron microscopy (SEM). The EDX technique detects X-rays emitted from the sample during bombardment by the SEM's electron beam; electrons are ejected from the atoms comprising the sample's surface. The resulting electron vacancies are filled by electrons from a higher state, and an X-ray is emitted to balance the energy difference between the two electrons' states. The EDS X-ray detector measures the relative abundance of emitted X-rays versus their energy. The surface topography of zeolite and catalyst was examined using Cambridge scanning electron microscope (S-360) at an accelerating voltage of 20 kV. Zeolite and catalyst samples were mounted on a double-sided tape attached to a metal stub and

sputtered with gold under argon vacuum in order to make the sample conductive.

2.4. Transesterification

Transesterification of palm oil into biodiesel was carried out in a 500 mL three-neck flask equipped with reflux condenser, temperature indicator, and controlled water bath heater. The reaction procedure is as follows: mixture of catalyst and methanol was heated to 60 °C under continuous stirring at 500 rpm. Subsequently, 125 mL of palm oil was added to the reactor. Molar ratio of palm oil and methanol used in this study was 1:7, and the amount of catalyst used was 3% weight of palm oil. Transesterification experiment was carried out at reaction time of 1 to 4 h. At the end of the reaction, the reactor was cooled to room temperature and the catalyst was separated from product mixture using vacuum filter.

The biodiesel product was separated from glycerol using funnel separator. Subsequently, the excess methanol was removed from the biodiesel product using vacuum rotary evaporator. Biodiesel product was then repeatedly washed using warm distilled water (60 °C). The fatty acid methyl ester or FAME layer (upper layer) was separated from water layer (bottom layer) using funnel separator. Some amount of sodium sulfate was added to the biodiesel product to remove residual water from the fatty acid methyl ester.

2.5. Determination and characterization of FAME contents

FAME content in biodiesel product was determined by gas chromatography analysis (GC Shimadzu 2014). The GC was equipped with a DB-Wax capillary column (30 m × 0.25 mm i.d. × 0.1 μm film thickness, Agilent JW Scientific) and flame ionization detector (FID). Helium was employed as carrier gas at 40 cm/s. The injector temperature was 250 °C at splitless condition. The FID was set at 300 °C. The initial oven temperature was set at 50 °C with equilibration time of 3 min. After isothermal period, oven temperature was increased to 250 °C at heating rate of 10 °C/min and held for 8 min. Peaks of methyl esters were identified by comparing them with the reference standard. The yield of biodiesel was determined by the following equation:

$$\text{Yield}(\%) = \frac{\text{weight of biodiesel} \times \% \text{FAME in sample}}{(\text{weight of palm oil}) \times 100\%} \quad (1)$$

where FAME is fatty acid methyl esters. Several physical properties of biodiesel product were also determined according to ASTM standard and the results were compared with the Indonesia National Standard for biodiesel. The kinematic viscosity was determined based on ASTM D445-10, 2010, while ASTM standard D.93, 2010 was employed for the determination of flash point. Cetane index and density/specific gravity of biodiesel were analyzed according to ASTM D.613, 2010, and ASTM D.1298, 2005, respectively.

Table 1
Fatty acid composition of palm oil.

Fatty acid	%
Lauric acid (C12:0)	0.8
Myristic acid (C14:0)	1.2
Palmitic acid (C16:0)	42.9
Palmitoleic acid (C16:1)	0.2
Stearic acid (C18:0)	4.7
Oleic acid (C18:1)	40.4
Linoleic acid (C18:2)	9.4
Linolenic acid (C18:3)	0.1
Arachidonic acid (C20:0)	0.3

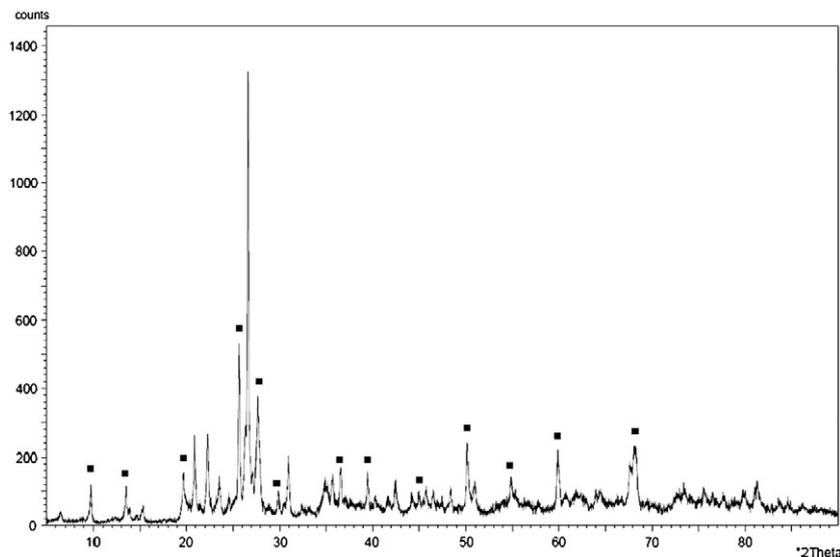


Fig. 1. The XRD pattern of raw zeolite.

3. Results and discussion

3.1. Characteristic of palm oil

The physical and chemical properties of palm oil were determined using standard test methods. These include density (ASTM D1298, 2005), kinematic viscosity (ASTM D445-10, 2010), free fatty acid content, and flash point (ASTM D93, 2010). The results were as follows: the density at 25 °C was 0.9016 g/cm³, kinematic viscosity at 23.4 °C was 70.9 cSt, free fatty acid and flash point were 0.02% and 220 °C, respectively. The chemical composition of palm oil used in this study was analyzed using gas chromatography (GC Shimadzu 2014) and the results are summarized in Table 1.

3.2. Catalyst characterisation

3.2.1. X-ray diffraction (XRD)

X-ray diffraction analysis was performed to identify the internal structure, bulk phase, and crystallinity of the catalyst. The XRD pattern

of raw zeolite is shown in Fig. 1. Fig. 1 shows the typical diffraction peaks of zeolite at Bragg angle (2θ) = 12.4°; 19.4°; 29.9°; 37.1°; 45°; 56°; and 60.6°. The pattern also indicates that the raw zeolite used in this study was classified into mordenite.

Fig. 2 depicts the XRD pattern of modified zeolite/catalyst. A new phase of K₂O can be observed at Bragg angle (2θ) = 31°; 39°; 51°; 55°; and 62°. During calcinations, molecules of potassium hydroxide in zeolite surface and matrix were transformed into K₂O. Potassium oxide (K₂O) is believed to play an important role during the transesterification of oil into fatty acid methyl esters since it has high catalytic activity.

3.2.2. Energy-dispersive X-ray spectrometry (EDX)

Potassium content in raw zeolite, modified zeolite/catalyst, and spent catalyst (after three reaction cycle) was determined using Energy-dispersive X-ray (EDX) spectrometry, and the results were 3.01% (weight) for raw zeolite, 45.34% and 43.80% for fresh catalyst (modified zeolite) and spent catalyst, respectively. The result showed that the potassium content on the modified zeolite increased after the impregnation with KOH. This indicates that potassium molecules

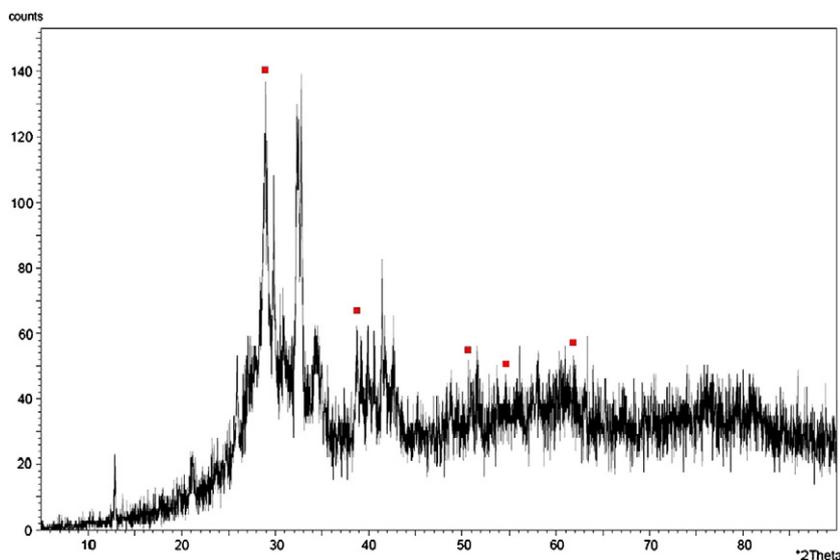


Fig. 2. XRD pattern of catalyst.

were attached or incorporated into zeolite structure or matrix during the impregnation process.

Reusability and stability of catalyst for biodiesel synthesis are very important for the industrial application. Potassium molecules should strongly attach on the structure of zeolite to make the catalyst stable. In order to examine the stability of catalyst, three consecutive reaction cycles using the same catalyst were conducted. After three reaction cycle test, the potassium content was also analyzed using EDX, and it was found that the potassium content in catalyst

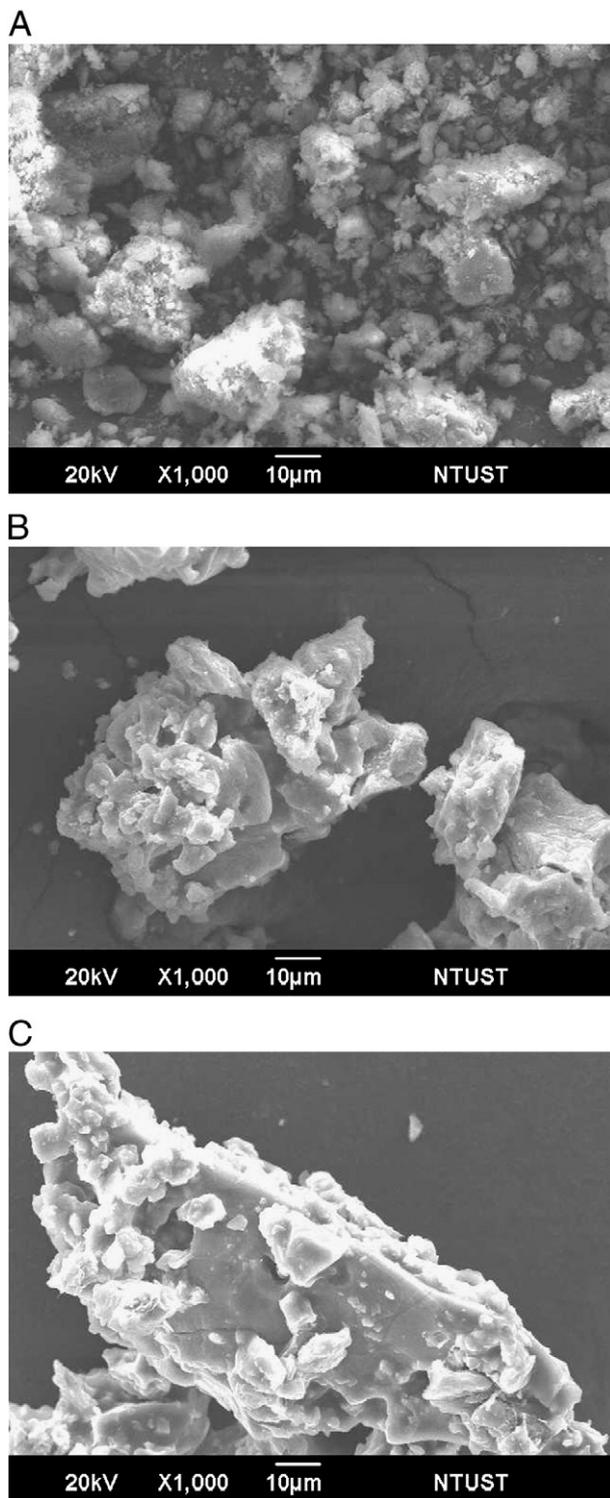


Fig. 3. SEM micrographs of (A) raw zeolite, (B) catalyst, and (C) spent catalyst after three reaction cycles.

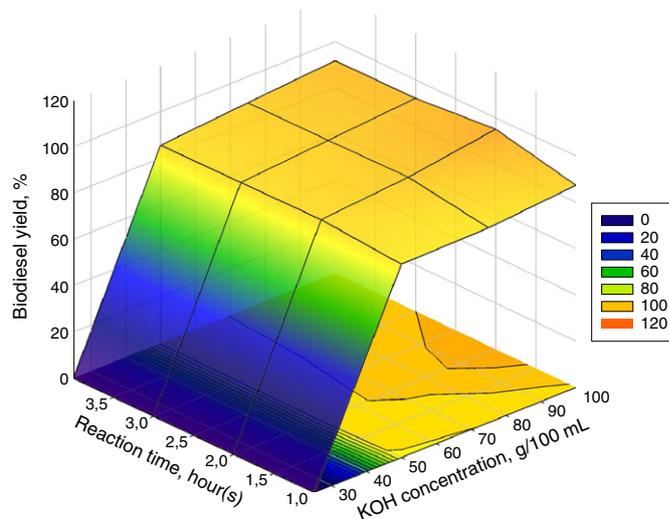


Fig. 4. The effect of catalyst loading and reaction time on the yield of biodiesel (reaction time between 1 and 4 h, amount of catalyst used was 3%, oil to methanol ratio 1:7, and reaction temperature 60 °C, KOH concentration for zeolite impregnation 25–100 g/100 mL).

decreased from 45.34% to 43.80%. This evidence indicates that the stability of catalyst is relatively good because only around 3.40% of the potassium content was leached during three reaction cycles.

3.2.3. Scanning electron microscopy (SEM)

The surface topography of raw zeolite, modified zeolite/catalyst, and spent catalyst (after three reaction cycles) was analyzed using scanning electron microscopy (SEM). The macrostructure of raw zeolite and its modified form remain intact after the calcination process, confirming the high thermal stability of zeolite (Fig. 3A and B). The surface topography of used catalyst also did not change significantly after reused for three reaction cycles (Fig. 3C).

3.3. Transesterification reaction

The transesterification of palm oil using KOH/zeolite as catalyst was performed under following conditions: catalyst amount 3%, ratio of palm oil to methanol 1:7, reaction temperature 60 °C, and stirring speed 700 rpm.

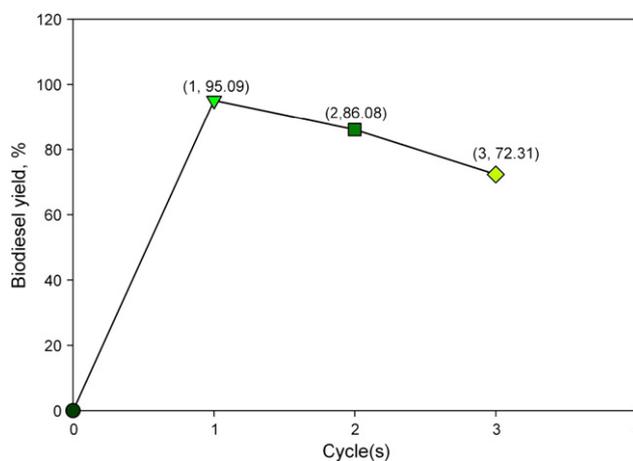


Fig. 5. Multiple cycle test of catalyst deactivation (impregnation with 100 g/100 mL KOH, reaction time 2 h, reaction temperature 60 °C, ratio of palm oil and methanol was 1:7, and 3% of catalyst amount).

Table 2

Comparison of the properties of biodiesel produced from palm oil with KOH/zeolite catalyst with the Indonesia National Standard (SNI-04-7182-2006).

Properties	Biodiesel produced	SNI
Density at 15 °C, g/mL	0.884 ± 0.00343	0.86–0.90
Kinematic viscosity at 40 °C, cSt	5.121 ± 0.221	1.9–6.0
Flash point, °C	170.417 ± 0.434	Min 65
Cetane number	58.500 ± 1.525	>45

3.3.1. Effect of KOH loading on biodiesel yield

To study the effect of potassium hydroxide (KOH) loading on the yield of biodiesel, a series of KOH/zeolite catalyst was prepared by impregnated zeolite with different concentration of KOH. The effect of KOH loading on the yield of biodiesel is shown in Fig. 4. This figure reveals that the yield of biodiesel increased with the increase of KOH loading. With the increased of KOH loading, the amount of KOH entering the structure of zeolite also increased. During the calcination process, KOH was converted into potassium oxide (K_2O) as shown in XRD pattern. As reported by Noiroj et al. (2009) and Soetaredjo et al. (2011), K_2O has a high catalytic performance for transesterification process. Along with the increased of KOH amount in the structure of zeolite, the formation of K_2O which acts as active sites for transesterification process was also increased, thus increased the yield of biodiesel.

3.3.2. Effect of reaction time on biodiesel yield

The effect of reaction time on the transesterification of palm oil into biodiesel was studied at reaction time between 1 and 4 h. The transesterification reaction consists of three step reactions to convert triglyceride to final product, methyl ester and glycerol. In the first

step, the triglycerides react with one molecule of alcohol, produce diglycerides and one molecule of ester. The molecule of diglycerides then reacts with another molecule of alcohol to produce monoglyceride and one molecule of ester. Finally, the reaction between monoglyceride and methanol produces methyl ester and glycerol. Therefore, it is important to select a proper transesterification time to ensure the completion of the reaction, especially if heterogeneous catalyst is used.

The effect of reaction time on the biodiesel produced is also depicted in Fig. 4. In the first hour of reaction, only some triglycerides were completely converted into fatty acid methyl ester (biodiesel). Furthermore, the rate of reaction was relatively slow in the first hour due to the problem of mixing and dispersion between palm oil and methanol (Freedman et al., 1986). With increasing of reaction time the amount of biodiesel produced also increased, and after 2 h of reaction time, the yield of biodiesel was essentially constant with time. The equilibrium condition of transesterification reaction of palm oil with methanol has been reached after 2 h.

3.3.3. Catalyst stability and reusability

The reusability and stability of heterogeneous catalyst are the most important criteria in the selection of appropriate catalyst for industrial application. Noiroj et al. (2009) mentioned that in heterogeneous catalyst application for biodiesel preparation, it is important to ensure that the active species are not leached from the solid support of the catalyst during the process. In this study, the reusability of KOH/zeolite catalyst was determined by carrying out three transesterification reaction cycles. The following reaction conditions were applied: reaction time of 2 h, palm oil to methanol molar ratio was 1:7, catalyst amount of 3% weight of palm oil, reaction temperature of 60 °C, and stirring speed was at 500 rpm.

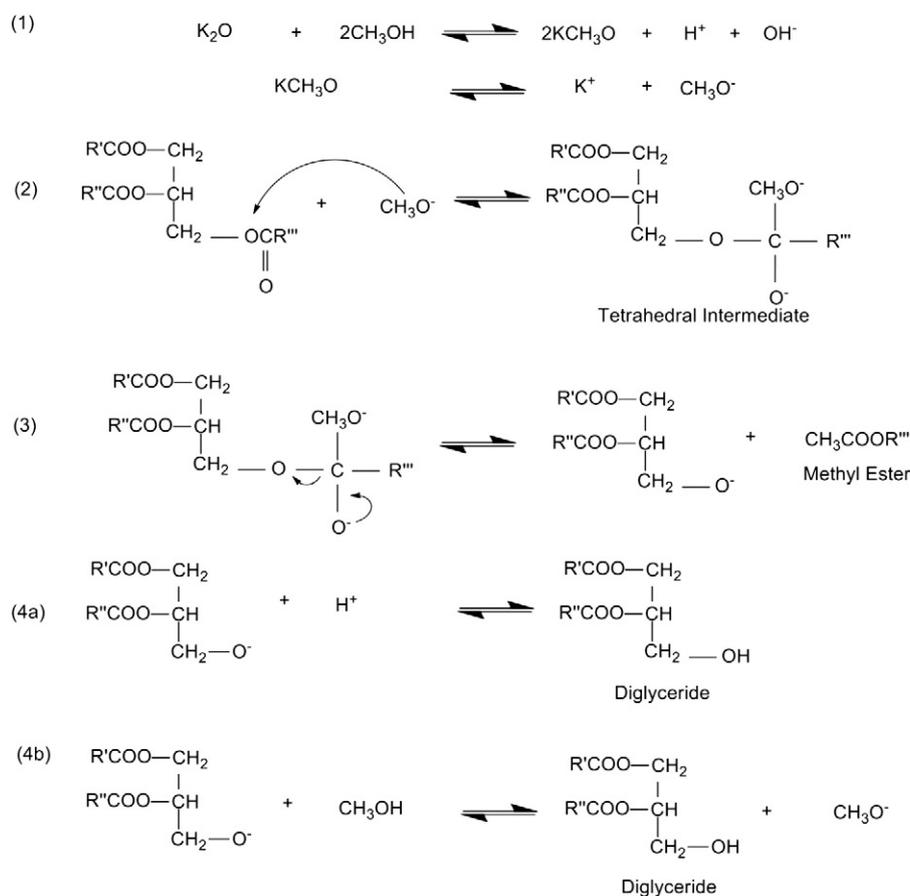


Fig. 6. Proposed reaction mechanism for transesterification of triglycerides using KOH/zeolite solid base catalyst.

For fresh catalyst (at KOH concentration of 100 g/100 mL) the maximum conversion was 95.09% as shown in Fig. 5. For subsequent reaction, the biodiesel yield was decreased to 86.08%, and for the third cycle the yield of biodiesel was just only 72.31% (Fig. 5). The decrease of biodiesel yield occurred because some of the active species in KOH/zeolite catalyst were leached or deactivated during transesterification reaction of palm oil with methanol. This phenomenon was supported by the EDX result which indicated that the potassium content in catalyst decreased from 45.34% to 43.80%.

3.4. Biodiesel characterisation

The physical and chemical properties (density, kinematic viscosity, flash point, and cetane number) of biodiesel produced by transesterification of palm oil with methanol using KOH/zeolite solid catalyst were determined by standard analysis as mentioned in Section 3.1 and the results were compared with the Indonesia National Standard for biodiesel, as shown in Table 2.

Since it affects the performance of injector, viscosity is the most important property of biodiesels; particularly at low temperatures when an increase in viscosity affects the fluidity of the fuel. The lower the viscosity of the biodiesel, the easier it is to pump and atomize and achieve finer droplets (Islam and Beg, 2004). The minimum value of flash point is required for safety and handling of the fuel. It is used to characterize the fire hazards of liquids. Since the flash point of biodiesel produced from this study is high (more than 60.5 °C), therefore, this fuel is safe for handling and storage for some period of time. With a high value of flash point, this biodiesel is considered as combustible.

Cetane number relates to the combustion quality of diesel fuel during compression ignition and also the ignition quality of diesel fuels. The cetane index of biodiesel obtained in this study is higher than conventional diesel fuel (45 to 55). This is due to the major contents of this fuel which are the methyl palmitate and methyl stearate which have the cetane index of 59.3 and 85.9, respectively (Rashid et al., 2011).

3.5. Proposed reaction mechanism

The transesterification reaction mechanism for biodiesel production using KOH/zeolite as catalysis is shown in Fig. 6. The mechanism is as follows: the first step of reaction is the formation of methoxide ion (CH_3O^-) from the reaction between the active site of catalyst (K_2O) with methanol. This methoxide ion is a strong base which has high catalytic activity in the transesterification reaction (Gryglewicz, 1999).

In the next step, the reactive methoxide ion attacks the carbonyl carbon atom of triglyceride leading to the formation of tetrahedral intermediate. Further rearrangement of tetrahedral intermediate produced one molecule of methyl ester and diglyceride anion. The reconstruction of diglyceride molecule began with the reaction with H^+ from the catalyst. On the other hand, the diglyceride anion may also react with methanol and generate reactive methoxide ion (Ma and Hanna, 1999). The catalytic reaction was then followed by the reaction between diglyceride and other methoxide ion to produce monoglyceride molecule and one molecule of methyl ester. Finally, carbonyl carbon atom of monoglyceride was attacked by methoxide ion producing one molecule of methyl ester and one molecule of glycerol.

4. Conclusion

Natural zeolite from Pacitan, East Java, Indonesia, was employed as catalyst support for biodiesel production. The catalyst was prepared by impregnating the zeolite with potassium hydroxide solution. The KOH

loaded zeolite was then calcined at 450 °C. During calcination, the KOH was converted into K_2O , which was believed to be the active site during the transesterification reaction. The maximum yield of biodiesel was 95.09%, and obtained at following operation condition: impregnation with 100 g/100 mL KOH, reaction time of 2 h, reaction temperature of 60 °C and ratio of palm oil and methanol was 1:7, and 3% weight of catalyst amount. During three cycles of transesterification reaction, 3.40% of active site of catalyst was leached from zeolite structure.

Acknowledgments

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