

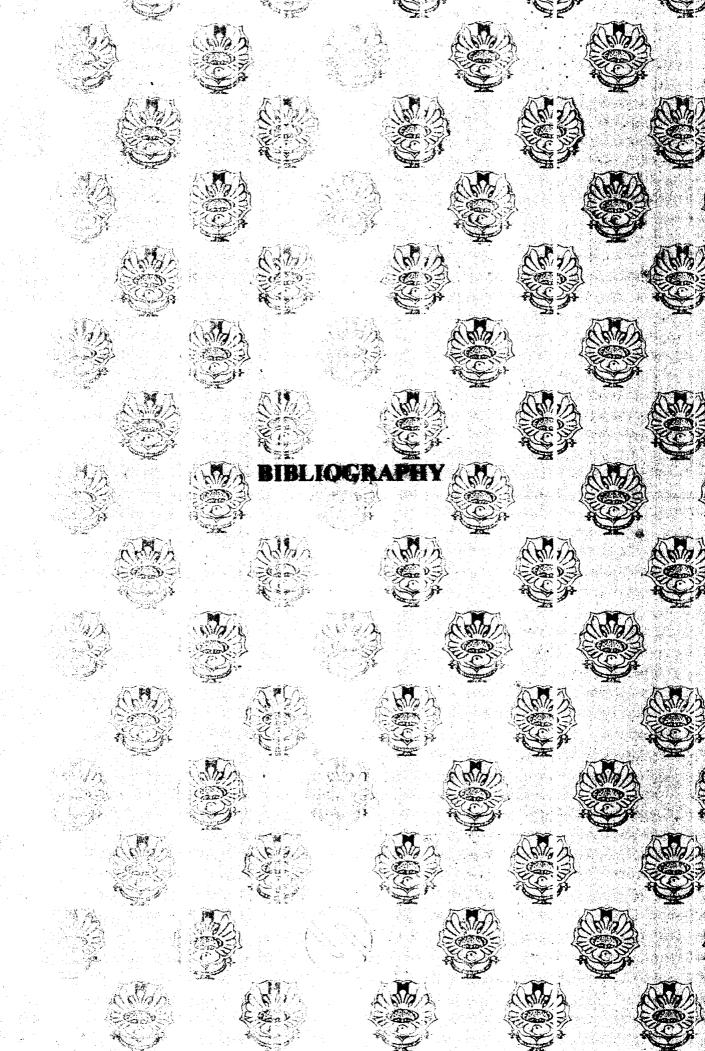
CHAPTER V

CONCLUSION

The catalytic cracking process conducted in this research follows the three-lump model fairly well and the reaction was found to be the first order. The predicted data calculated using the model is comparable with the data obtained from the experiment. The deviation of the calculated and experimental data is quite small, less than 10%. Using this model, the rate constant values for the catalytic cracking reaction are:

- 9.3964, 1.7581, and 0.4732 h⁻¹ for reaction temperature of 623.15 K
- 20.0346, 3.5761, and 0.5977 h^{-1} for reaction temperature of 673.15 K
- 28.2084, 5.1278, and 0.6639 h^{-1} for reaction temperature of 723.15 K

Using the Arrhenius equation, the activation energy is 41.49, 40.36 and 12.78 kJ/mol for E_1 , E_2 , and E_3 , respectively. These values of activation energy are valid from reaction temperature of 623.15 K until 723.15 K.



BIBLIOGRAPHY

- 1. Kloprogge, J.T., L.V. Duong, and R.L. Frost, A Review of The Synthesis and Characterisation of Pillared Clays and Related Porous Materials for Cracking of Vegetable Oils to Produce Biofuels. Environ. Geol., 2005. 47: p. 967-981.
- 2. Ooi, Y.S., et al., Catalytic Conversion of Palm Oil-Based Fatty Acid Mixture to Liquid Fuel. Bimass and Bioenergy, 2004. 27: p. 477-484.
- 3. Ooi, Y.S., et al., Synthesis of Composite Material MCM-41/Beta and Its Catalytic Performance in Waste Used palm Oil Cracking. Applied Catalysis A: General, 2004. 274: p. 15-23.
- Twaiq, F.A., A.R. Mohamed, and S. Bhatia, Liquid Hydrocarbon Fuels from Palm Oil by Catalytic Cracking over Aluminosilicate Mesoporous Catalysts with Various Si/Al Ratios. Microporous and Mesoporous Materials, 2003. 64: p. 95-107.
- 5. Nasikin, M., A. Wahid, and G. Iswara, Perengkahan Katalitik Fasa Cair Minyak Sawit Menjadi Biogasolin, in Seminar Nasional Teknik Kimia Indonesia 2006. 2006: Palembang, Indonesia. p. KKR 08-1-5.
- 6. Twaiq, F.A., et al., Catalytic Conversion of Palm Oil over Mesoporous Aluminosilicate MCM-41 for The Production of Liquid Hydrocarbon Fuels. Fuel Processing Technology, 2003. 84: p. 105-120.
- 7. Twaiq, F.A.A., A.R. Mohamad, and S. Bhatia, Performance of Composite Catalysts in Palm Oil Cracking for The Production of Liquid Fuels and Chemicals. Fuel Processing Technology, 2004. 85: p. 1283-1300.
- 8. Ooi, Y.S., et al., Catalytic Conversion of Fatty Acids Mixture to Liquid Fuels over Mesoporous Materials. React. Kinet. Catal. Lett, 2005. 84: p. 295-302.
- 9. Ooi, Y.S., et al., Catalytic Cracking of Used Palm Oil and Palm Oil Fatty Acids Mixture for the Production of Liquid Fuel: Kinetic Modeling. J. Am. Chem. Soc, 2004. 18: p. 1555-1561.
- 10. Ooi, Y.S., et al., Catalytic Conversion of Fatty Acids Mixture to Liquid Fuel and Chemicals over Composite Microporous/Mesoporous Catalysts. J. Am. Chem. Soc, 2005. 19: p. 736-743.
- 11. Wibisono, N., Synthesis of Periodic Mesoporous Organosilica MCM-41 using Vesicle Templating Method. 2007, Widya Mandala Catholic University Surabaya: Surabaya.
- 12. Siswanto, D.Y. and G.W. Salim, Catalytic Cracking of Palm Oil for the Production of Liquid Hydrocarbon Fuel Using MCM-41. 2007.
- 13. Hamm, W. and R.J. Hamilton, *Edible Oil Processing*. 2000, Sheffield: Sheffield Academic Press.
- 14. Ito, S. World Food Statistics and Graphics. [cited 2007 1st November].
- 15. Wikipedia1.
- 16. Maher, K.D., Bressler, D.C, Pyrolisis of Triglyceride Materials for The Production of Renewable Fuels and Chemicals. Bioresourse Technology 2006. 98: p. 2351-2368.
- 17. Meng, X.X., C. Gao, J. Li.L., *Catalytic Pyrolisis of Heavy Oils* :8-Lump *Kinetic Model*. Applied Catalysis A General 2006. **31**: p. 32-38.
- 18. Blin, J.L., et al., *Kinetic Study of MCM-41 Synthesis*. International Journal of Inorganic Materials, 2001. 3: p. 75-86.

- 19. Lin, W., et al., New Mineralization Agents for the Synthesis of MCM-41. J. Microporous and Mesoporous Materials, 1999. 33: p. 187-196.
- 20. Grun, M., et al., Novel Pathways for the Preparation of Mesoporous MCM-41 Materials: Control of Porosity and Morphology. J. Microporous and Mesoporous Materials, 1999. 27: p. 207-216.
- 21. Sonwane, C.G. and S.K. Bhatia, *Structural Characterization of MCM-41 over* a Wide Range of Length Scales. Langmuir, 1999. 15: p. 2809-2816.
- 22. Kresge, C.T., et al., Ordered Mesoporous Molecular Sieves Synthesized by a Liquid Crystal Template Mechanism. Nature, 1992. 359: p. 710-712.
- 23. Chen, H. and Y. Wang, Preparation of MCM-41 with High Thermal Stability and Complementary Textural Porosity. J. Ceramics International, 2002. 28: p. 541-547.
- 24. Do, D.D., Practical Approaches of Pure Component Adsorption Equilibria, in Adsorption Analysis: Equilibria and Kinetics. 1998: p. 112-113, 142-143.
- 25. Charusiri, W. and T. Vitidsant, *Kinetic Study of Used Vegetable Oil to Liquid Fuels over Sulfated Zirconia.* J. Am. Chem. Soc, 2005. **19**: p. 1783-1789.
- 26. Demirbas, A., Fuel conversional aspects of palm oil and sunflower oil. Energy sources, 2003. 25: p. 457-466.
- 27. Leng, T.Y.M., A.R., Bhatia, S, Catalytic Conversion of Palm Oil to Fuels and Chemicals. Canadian Journal of Chemical Engineering, 1999. 77: p. 157-162.
- 28. Appleby, W.G.G., J.W. and Good, M, Coke Formation in Catalytic Cracking. Ind. Eng.Chem. Res., 1962. 1: p. 102-110.
- 29. Juarez, J.A., Isunza, F.L, Rodriguez, E.A. and Mayorga, J.C.M, A Strategy for Kinetic Parameter Estimation in The Fluid Catalytic Cracking Process. Ind. Eng. Chem. Res., 1997. 36: p. 5170-5174.